

Leaving Equilibrium Assumptions Behind Challenges

Motivation

Modelling Non-Equilibrium

- Limits of *thermodynamic equilibrium assumption*
 - confidence in existing models
- Being able to model situation of clear non-equilibrium
 - extending range of applicability

Current Work

Thermal Non-Equilibrium

$$\begin{aligned} \frac{\partial(\phi \rho_w S_w u_w)}{\partial t} + \nabla \cdot (\rho_w \mathbf{v}_w h_w + \sum_{\kappa} \mathbf{j}_w^{\kappa} h_w^{\kappa}) - \nabla \cdot (\phi S_w \lambda_w \nabla T_w) = \\ + \text{Nu}(\text{Re}, \text{Pr}) a_{wn} \frac{\bar{\lambda}_{wn}}{L} (T_n - T_w) + \text{Nu}(\text{Re}, \text{Pr}) a_{ws} \frac{\bar{\lambda}_{ws}}{L} (T_s - T_w) \\ + \sum_{\kappa} q_{\kappa \rightarrow w} h_{\kappa}^{\text{origin}} + q_w^{\text{energy}} \end{aligned}$$

$$\begin{aligned} \frac{\partial(\phi \rho_n S_n u_n)}{\partial t} + \nabla \cdot (\rho_n \mathbf{v}_n h_n + \sum_{\kappa} \mathbf{j}_n^{\kappa} h_n^{\kappa}) - \nabla \cdot (\phi S_n \lambda_n \nabla T_n) = \\ - \text{Nu}(\text{Re}, \text{Pr}) a_{wn} \frac{\bar{\lambda}_{wn}}{L} (T_n - T_w) + \text{Nu}(\text{Re}, \text{Pr}) a_{ns} \frac{\bar{\lambda}_{ns}}{L} (T_s - T_n) \\ + \sum_{\kappa} q_{\kappa \rightarrow n} h_{\kappa}^{\text{origin}} + q_n^{\text{energy}} \end{aligned}$$

$$\begin{aligned} \frac{\partial((1-\phi) \rho_s c T_s)}{\partial t} - \nabla \cdot ((1-\phi) \lambda_s \nabla T_s) = \\ - \text{Nu}(\text{Re}, \text{Pr}) a_{ws} \frac{\bar{\lambda}_{ws}}{L} (T_s - T_w) - \text{Nu}(\text{Re}, \text{Pr}) a_{ns} \frac{\bar{\lambda}_{ns}}{L} (T_s - T_n) + q_s^{\text{energy}} \end{aligned}$$

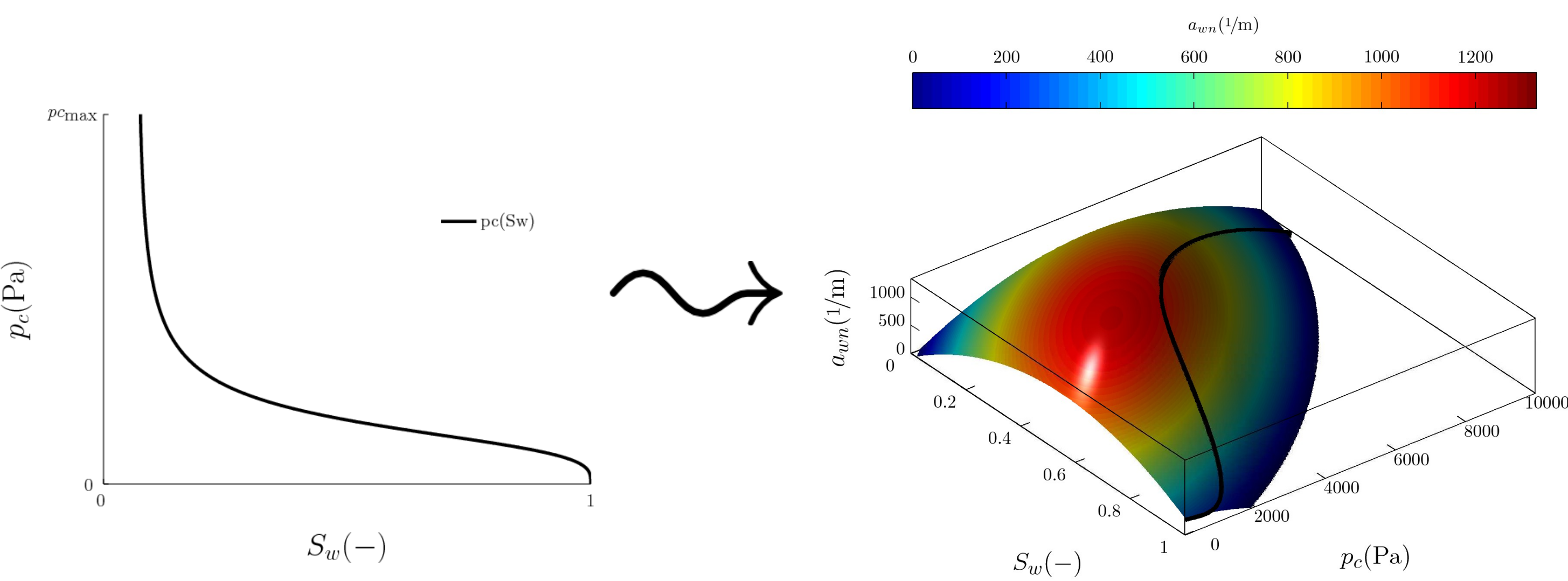


Figure 1: Capillary pressure - saturation relationship (left), capillary pressure - saturation - interfacial area relationship (right)

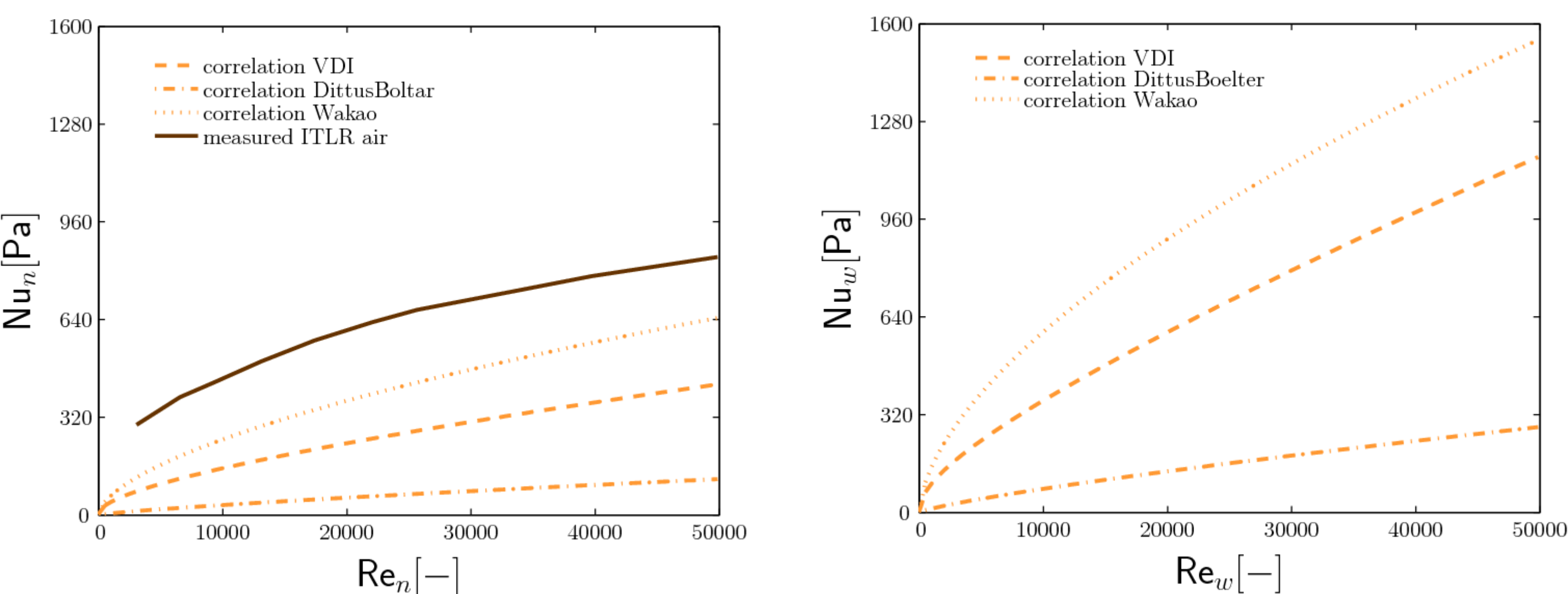


Figure 2: Nusselt Correlations water (left), Nusselt Correlations air (right)

Standard Energy Equation

$$\begin{aligned} \frac{\partial((1-\phi) \rho_s c T)}{\partial t} + \sum_{\alpha} \frac{\partial(\phi \rho_{\alpha} S_{\alpha} u_{\alpha})}{\partial t} - \nabla \cdot (\bar{\lambda}_{\text{pm}} \nabla T) \\ + \sum_{\alpha} \nabla \cdot (\rho_{\alpha} \mathbf{v}_{\alpha} h_{\alpha} + \sum_{\kappa} \mathbf{j}_{\alpha}^{\kappa} h_{\alpha}^{\kappa}) = 0 \end{aligned}$$

Challenges

Volume changing work

$$\dot{m} = 0.1 \text{ kg/s} \rightarrow \begin{cases} S_{wi} = 1, T_i = 290 \text{ K} \\ p_{wi} = 0.1 \text{ MPa} \end{cases} \quad \begin{matrix} S_{wD} = S_{wi}, T_D = T_i \\ p_{wD} = p_{wi} \end{matrix}$$

$\dot{h} = h(0.1 \text{ kg/s}, 290 \text{ K})$

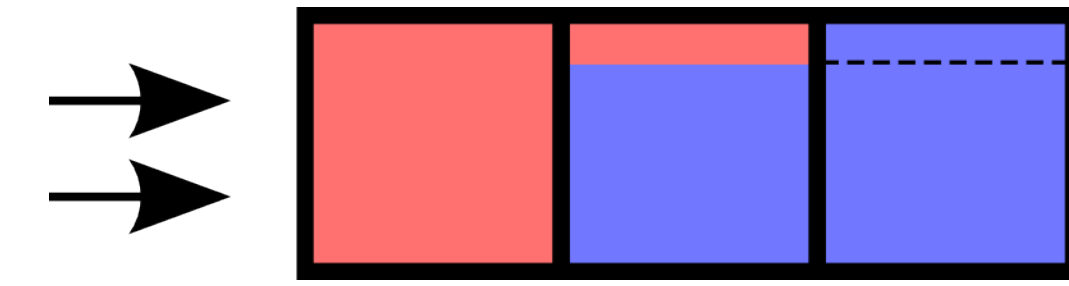
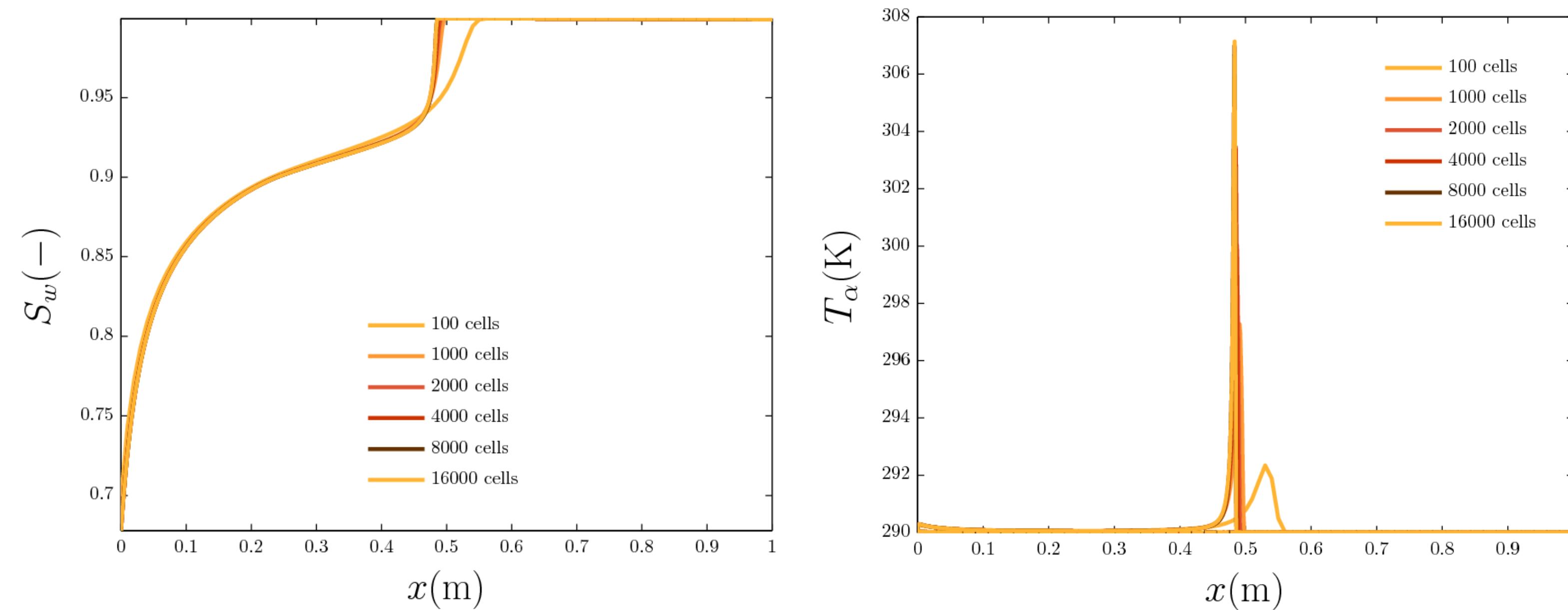


Figure 2: Schematic of the simulation setup (top), convergence study (middle), helper cartoon (bottom)

$$\sum_{\alpha} \frac{\partial(\phi \rho_{\alpha} S_{\alpha} u_{\alpha})}{\partial t} + \sum_{\alpha} (\mathbf{v}_{\alpha} \rho_{\alpha} h_{\alpha}) = 0$$

$$\frac{\partial(\phi \rho_w S_w u_w)}{\partial t} + (\mathbf{v}_w \rho_w h_w) = Q_{n \rightarrow w}$$

$$\frac{\partial(\phi \rho_n S_n u_n)}{\partial t} + (\mathbf{v}_n \rho_n h_n) = Q_{w \rightarrow n}$$

Enthalpy of solvation

- When mass changes from one phase to another, there is an energy change associated with it.
- Where do I find the data?

Visualization of Temperature in Micro model

- There are existing Micro models.
- How to measure temperature distribution?

Sensitivity Analysis

- Many new parameters are in the model
- How to find out which one needs most attention?

Scenarios

- Up to now rather academic examples have been simulated.
- Ideas for more realistic setting welcomed!

Indicators

- It would be nice to know when a model is leaving it's range of validity
- As little limitations / assumptions should go into the development of these indicators

Outlook

Identify Need for Complex Model

- Under which circumstances is thermodynamic equilibrium a good assumption?
- Sensitivity Analysis: Which Parameters / choices have most influence?